\section*{spirax sarco

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PTF4

# PTF4 <br> <br> <br> Pivotrol ${ }^{\circledR}$ Pump (patented) $\subset \in$ version <br> <br> <br> Pivotrol ${ }^{\circledR}$ Pump (patented) $\subset \in$ version Dual Mechanism - Pressure Powered Pump 

} Dual Mechanism - Pressure Powered Pump}}

Cross sectional view


## Description

The Spirax Sarco Pivotrol ${ }^{\circledR}$ Pump (patented) is a non electric pump which transfers high temperature condensate, or other liquids from a low point, low pressure or vacuum space to an area of higher pressure or elevation. This self-contained unit including PowerPivot ${ }^{\circledR}$ technology (patented) uses steam, compressed air or any other suitable pressurised gas as the pumping force.
The standard Pivotrol ${ }^{\circledR}$ PTF4 Pump will handle liquids from 0.88 to 1.0 specific gravity.

## Compliance

This product fully complies with the requirements of the European Pressure Equipment Directive 97/23/EC and is certified for use to Category III within Group 2 Gases and to SEP for Group 2 liquids. The product carries the $\mathbb{C} \in$ mark when so required.
This product is designed and built to the pressure vessel code ASME Section VIII, Division 1.
Accessories: Reflex type gauge glass - Insulation cover.
Operating characteristics
Pump discharge per cycle
102.1 litres (26.9 US gal)

Maximum instantaneous discharge rate 28 litres/s (450 US gpm)
Steam consumption See page 8

Average air consumption See page 8

For increased service life - Operate the pump with a motive pressure of 1.03 to 1.37 bar g ( 15 to 20 psi g ) above the pump backpressure.

## Sizes and pipe connections

| Inlet and Outlet: | DN100 x DN100 Flanged ASME Class 150, <br> $4 " \times 4 "$ Screwed NPT and Socket weld |
| :--- | :--- |
| Motive and Exhaust: | $4 " \times 4 "$ Screwed NPT and Socket weld |

Motive and Exhaust: 4" x 4" Screwed NPT and Socket weld

First for Steam Solutions

## Materials

| No. | Part | Material |  |
| :--- | :--- | :--- | ---: |
| $\mathbf{1}$ | Body | Fabricated |  |
| $\mathbf{2}$ | Cover | Cast steel $\quad$ ASTM code stamped |  |
| $\mathbf{3}$ | Cover gasket | Spiral wound AISI 304/Graphite |  |
| $\mathbf{4}$ | Steam inlet valve assembly | Stainless steel |  |
| $\mathbf{5}$ | Steam inlet valve gasket | Stainless steel |  |
| $\mathbf{6}$ | Exhaust valve assembly | Stainless steel |  |
| $\mathbf{7}$ | Exhaust valve gasket | Stainless steel |  |
| $\mathbf{8}$ | Eye bolt | Stainless steel |  |
| $\mathbf{9}$ | Pushrod assembly | Stainless steel |  |
| $\mathbf{1 0}$ | Mechanism support | Stainless steel |  |
| $\mathbf{1 1}$ | Bushing mounting plate | Stainless steel |  |
|  | Bushings | Carbide |  |
| $\mathbf{1 2}$ | Spring anchor | Carbide |  |
| $\mathbf{1 3}$ | Spring | Inconel |  |
| $\mathbf{1 4}$ | Float arm assembly | Stainless steel |  |
| $\mathbf{1 5}$ | Pivots | Float pivot | Stainless steel |
| $\mathbf{1 6}$ | Pin | Stainless steel |  |
| $\mathbf{1 7}$ | Paddle | Stainless steel |  |
| $\mathbf{1 8}$ | Float | Stainless steel |  |
| $\mathbf{1 9}$ | Screws (typical) | Stainless steel |  |
| $\mathbf{2 0}$ | Plugs (typical) | Forged stainless steel |  |
| $\mathbf{2 1}$ | Check valves (SDCV44) | Stainless steel |  |
| $\mathbf{2 2}$ | Cycle counter | Various |  |
| $\mathbf{2 3}$ | Vent assist valve | Stainless steel |  |
|  |  |  |  |

## Pressure / temperature limits



The product must not be used in this region.

| Body design condition |  | ASME Section VIII, Division 1 |
| :---: | :---: | :---: |
| PMA Maximum allowable pressure | 13.8 bar g @ 204º | (200 psi g @ 400%) |
| TMA Maximum allowable temperature | $343^{\circ} \mathrm{C}$ @ 8.6 bar g | (650% @ 125 psig ) |
| Minimum allowable temperature | $-28.9^{\circ} \mathrm{C}$ | $\left(-20^{\circ} \mathrm{F}\right)$ |
| PMO Maximum operating pressure | 13.8 bar g | (200 psi g) |
| TMO Maximum operating temperature for saturated steam service | $198^{\circ} \mathrm{C}$ | $\left(388^{\circ} \mathrm{F}\right)$ |
| Minimum operating temperature <br> Note: For lower operating temperatures consult Spirax Sarco | $-28.9^{\circ} \mathrm{C}$ | (-20 ${ }^{\circ} \mathrm{F}$ ) |
| Minimum motive differential required: | 0.5 bar g | (7 psi g) |
| Maximum backpressure: |  | 75\% of motive pressure |
| Designed for a maximum cold hydraulic test pressure of: | 20.7 bar g | (300 psi g) |
| Note: With internals fitted, test pressure must not exceed: | 20.7 bar g | (300 psi g) |

Specific gravity of pumped liquid 0.88 to 1.0
Cycle counter: For further technical information about the cycle counter contact Spirax Sarco or your local Spirax Sarco representative.

## Filling head requirements

| Filling head | Filling head above pump cover | Filling height from base of pump |
| :--- | :---: | ---: |
| Standard recommended | $305 \mathrm{~mm} \mathrm{(12")}$ | $\left.1125 \mathrm{~mm} \mathrm{(44.3}^{\prime \prime}\right)$ |
| Maximum filling head | $1524 \mathrm{~mm} \mathrm{(60")}$ | 2337 mm (92.0") |
| Minimum filling head | $-76 \mathrm{~mm} \mathrm{(-3")}$ | 744 mm (29.3") |

[^0]Dimensions (approximate) in millimetres and (inches)

| Dimension | A | B | C | D | E | F | G | H | I | J | K | L | M | N |
| :--- | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| millimetres | 1002 | 851 | 813 | 368 | 406 | 503 | 508 | 267 | 15 | 699 | 800 | 1427 | 102 | 224 |
| Inches | $(39.5)$ | $(33.5)$ | $(32.0)$ | $(14.5)$ | $(16.0)$ | $(19.8)$ | $(20.0)$ | $(10.5)$ | $(0.6)$ | $(27.5)$ | $(31.5)$ | $(56.2)$ | $(4.0)$ | $(8.8)$ |

Weights (approximate) in kgs (lbs)

| PTF4 complete unit weight | $249.0 \mathrm{~kg}(550 \mathrm{lb})$ |
| :--- | ---: |
| Reflex gauge glass weight - Each | $10.4 \mathrm{~kg} \quad(23 \mathrm{lb})$ |
| Cover and mechanism assembly weight - Each | $29.5 \mathrm{~kg} \quad(65 \mathrm{lb})$ |

$12 \mathrm{~mm}\left(1 / 22^{\prime \prime}\right)$ NPT / SW motive inlet

25 mm (1") NPT / SW exhaust valve


Pressure gauges may be fitted to any of the top gauge glass connections


## Condensate pumps

Mechanical pumps and pumps traps

## Recommended installation

The pump is fitted with a vented receiver or an inlet reservoir.
Details of the application will determine whether a vented receiver or an inlet reservoir will be needed


## Sizing and selection

## How to size and select

From the inlet pressure, backpressure and filling head conditions given below, select the pump size and check valve package which meets the capacity requirement of the application.
Specify pump body - Type PTF4. Select optional extras as required.
For $\mathrm{kg} / \mathrm{h}$, multiply the capacities below by 0.454 (For gpm, multiply the capacities below by 0.002).
Backpressure in bar $g=$ lift height $(H)$ in metres divided by 10 plus the pressure in the return line (Backpressure in psi $g=$ lift height $(\mathrm{H})$ in feet $\times 0.433$ plus the pressure in the return line). Added to this is the downstream piping friction pressure drop in bar g (psi g) calculated and based on the maximum instantaneous discharge rate of the respective pump selected - See TI sheets.

Note: To achieve rated capacity, the pump must be installed with check valves supplied by Spirax Sarco. Use of a substitute check valve may affect the performance of the pump.
Capacity lb/h when installed with the recommended filling head above the top of the pump.

| $\qquad$Condensate load $9545 \mathrm{~kg} / \mathrm{h}$ <br> $(21000 \mathrm{lb} / \mathrm{h})$  <br> Steam pressure available for operating pump 5.5 barg | $(80 \mathrm{psig})$ |  |
| ---: | :--- | :--- |
| Vertical lift from pump to the return piping | 9.1 m | $(30 \mathrm{feet})$ |
| Pressure in the return piping (piping friction negligible) | 1.7 barg | $(25 \mathrm{psig})$ |
| Filling head on the pump available | 610 mm | $\left(24{ }^{\prime \prime}\right)$ |

## Solution:

1. Calculate ' $\mathbf{H}$ ', the total lift or backpressure, against which the condensate must be pumped:
'H' Metric $=(9.1 \mathrm{~m} / 10)+1.7$ bar g = 2.6 bar g
'H' Imperial $=(30$ feet $\times 0.433)+25 \mathrm{psi} \mathrm{g}=38 \mathrm{psi} \mathrm{g})$
2. From the capacity table, given an inlet pressure of 5.5 bar $\mathrm{g}(80 \mathrm{psig})$ and a backpressure of 2.8 bar $\mathrm{g}(40 \mathrm{psig})$, choose a PTF4 pump with stainless steel check valves, which has a capacity of $12264 \mathrm{~kg} / \mathrm{h}(26980 \mathrm{lb} / \mathrm{h})$.

Note from capacity multiplying factor charts:
A. If filling head were $457 \mathrm{~mm}(18 ")$ PTF4 pump capacity would be: $=0.98 \times 12264 \mathrm{~kg} / \mathrm{h}(26980 \mathrm{lb} / \mathrm{h})=12018 \mathrm{~kg} / \mathrm{h}(26441 \mathrm{lb} / \mathrm{h})$
B. Pump capacity using compressed air would be (\% backpressure is 5.5 to 2.6 bar g ( 38 to 80 psig ) $=47 \%$ e.g. use $50 \%$ ):
$=1.85 \times 12264 \mathrm{~kg} / \mathrm{h}(26980 \mathrm{lb} / \mathrm{h})=22688 \mathrm{~kg} / \mathrm{h}(49914 \mathrm{lb} / \mathrm{h})$.

## Intended use

This product fully complies with the requirements of the European Pressure Equipment Directive $97 / 23 / E C$ and is certified for use to Category III within Group 2 Gases and to SEP for Group 2 liquids. The product carries the CE mark when so required. This product is designed and built to the pressure vessel code ASME section VIII Division 1.

## Vented receiver (open system)

To drain condensate from a single or multiple source an 'open system', a vented receiver should be installed in a horizontal plane above and ahead of the pump. Sufficient receiver volume is needed above the filling head level to accept the condensate reaching the receiver during the pump discharge stroke. More important, the receiver must be sized to allow sufficient area for complete flash steam separation from the condensate. The Table below displays the proper vented receiver sizing (per criteria set forth in the A.S.H.R.A.E. Handbook) based on the amount of flash steam present. If the receiver is sized as shown below, there will be sufficient volume for condensate storage and sufficient area for flash steam separation. The receiver can be a length of large diameter pipe or a tank.

## Pump size

| Flash steam up to: | Pipe size |  | Vent line Diameter |
| :---: | :---: | :---: | :---: |
|  | Diameter | Length |  |
| $\begin{gathered} 454 \mathrm{~kg} / \mathrm{h} \\ (1000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ | 400 mm (16") | $\begin{gathered} 1524 \mathrm{~mm} \\ (60 ") \end{gathered}$ | 150 mm <br> (6") |
| $\begin{gathered} 907 \mathrm{~kg} / \mathrm{h} \\ (2000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ | 500 mm (20") | $\begin{gathered} 1524 \mathrm{~mm} \\ (60 ") \end{gathered}$ | 200 mm <br> (8") |
| $\begin{gathered} 1361 \mathrm{~kg} / \mathrm{h} \\ (3000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ | 600 mm (24") | $\begin{gathered} 1524 \mathrm{~mm} \\ (60 ") \end{gathered}$ | 200 mm <br> (8") |
| $\begin{gathered} 1814 \mathrm{~kg} / \mathrm{h} \\ (4000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ | $650 \mathrm{~mm}$ $\left(26^{\prime \prime}\right)$ | $\begin{gathered} 1524 \mathrm{~mm} \\ \left(60^{\prime}\right) \\ \hline \end{gathered}$ | $250 \mathrm{~mm}$ <br> (10") |
| $\begin{gathered} 2268 \mathrm{~kg} / \mathrm{h} \\ (5000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ | $700 \text { mm }$ (28") | $\begin{gathered} 1524 \mathrm{~mm} \\ (60 ") \end{gathered}$ | $250 \mathrm{~mm}$ (10") |
| $\begin{gathered} 2722 \mathrm{~kg} / \mathrm{h} \\ (6000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ | 750 mm (30") | $\begin{gathered} 1829 \mathrm{~mm} \\ (72 ") \end{gathered}$ | 300 mm (12") |
| $\begin{gathered} 3175 \mathrm{~kg} / \mathrm{h} \\ (7000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ | $800 \text { mm }$ (32") | $\begin{gathered} 1829 \mathrm{~mm} \\ (72 ") \end{gathered}$ | 300 mm (12") |
| $\begin{gathered} 3629 \mathrm{~kg} / \mathrm{h} \\ (8000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ | 900 mm (36") | $\begin{gathered} 1829 \mathrm{~mm} \\ \left(72^{\prime \prime}\right) \end{gathered}$ | 350 mm (14") |

## Inlet reservoir piping (closed system)

To drain condensate from a single piece of equipment in a 'closed system', a reservoir should be installed in a horizontal plane above and ahead of the pump. Sufficient reservoir volume is needed above the filling head level to accept the condensate reaching the reservoir during the pump discharge stroke. The Table below displays the minimum reservoir sizing, based on a condensate load, needed to prevent equipment flooding during the pump dischare stroke. The reservoir can be a length of large diameter pipe or a tank.

## Pump size

| Liquid load | Reservoir pipe size* |  |  |  |
| :---: | :---: | :---: | :---: | :---: |
| $\begin{gathered} \mathrm{kg} / \mathrm{h} \\ (\mathrm{lb} / \mathrm{h}) \end{gathered}$ | 300 mm (12") | 400 mm (16") | 500 mm (20") | 600 mm <br> (24") |
| $\begin{gathered} 4535 \mathrm{~kg} / \mathrm{h} \\ (10000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ | $\begin{gathered} 1524 \mathrm{~mm} \\ (5 \mathrm{ft}) \end{gathered}$ | $\begin{gathered} 914 \mathrm{~mm} \\ (3 \mathrm{ft}) \end{gathered}$ | $\begin{gathered} 610 \mathrm{~mm} \\ (2 \mathrm{ft}) \end{gathered}$ |  |
| $\begin{gathered} 9070 \mathrm{~kg} / \mathrm{h} \\ (20000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ | $\begin{gathered} 3048 \mathrm{~mm} \\ (10 \mathrm{ft}) \end{gathered}$ | $\begin{gathered} 2133 \mathrm{~mm} \\ (7 \mathrm{ft}) \end{gathered}$ | $\begin{gathered} 1219 \mathrm{~mm} \\ (4 \mathrm{ft}) \end{gathered}$ |  |
| $\begin{gathered} 13605 \mathrm{~kg} / \mathrm{h} \\ (30000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ |  | $\begin{gathered} 2743 \mathrm{~mm} \\ (9 \mathrm{ft}) \end{gathered}$ | $\begin{gathered} 1828 \mathrm{~mm} \\ (6 \mathrm{ft}) \end{gathered}$ | $\begin{gathered} 1219 \mathrm{~mm} \\ (4 \mathrm{ft}) \end{gathered}$ |
| $\begin{gathered} 18141 \mathrm{~kg} / \mathrm{h} \\ (40000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ |  | $\begin{gathered} 3658 \mathrm{~mm} \\ (12 \mathrm{ft}) \end{gathered}$ | $\begin{gathered} 2286 \mathrm{~mm} \\ (7.5 \mathrm{ft}) \end{gathered}$ | $\begin{gathered} 1828 \mathrm{~mm} \\ (6 \mathrm{ft}) \end{gathered}$ |
| $\begin{gathered} 22676 \mathrm{~kg} / \mathrm{h} \\ (50000 \mathrm{lb} / \mathrm{h}) \end{gathered}$ |  |  | $\begin{gathered} 2743 \mathrm{~mm} \\ (9 \mathrm{ft}) \end{gathered}$ | $\begin{gathered} 1828 \mathrm{~mm} \\ (6 \mathrm{ft}) \end{gathered}$ |
| $\begin{array}{r} 27211 \mathrm{~kg} / \mathrm{h} \\ (60000 \mathrm{lb} / \mathrm{h}) \end{array}$ |  |  | $\begin{gathered} 2743 \mathrm{~mm} \\ (9 \mathrm{ft}) \end{gathered}$ | $\begin{gathered} 1828 \mathrm{~mm} \\ (6 \mathrm{ft}) \end{gathered}$ |

* When the backpressure or motive pressure is less than $50 \%$, these reservoir lengths can be reduced by half.


## Multiplying factors for non-standard conditions

| Filling head |  | Capacity multiplying factors for non-standard filling heads |
| :---: | :---: | :---: |
| mm | inches |  |
| -76 | (-3") | 0.23 |
| -25 | (-1") | 0.41 |
| 0 | (0) | 0.70 |
| 152 | (6") | 0.89 |
| 305 | (12") | 0.95 |
| 457 | (18") | 0.98 |
| 610 | (24") | 1.00 |
| 914 | (36") | 1.00 |
| 1219 | (48") | 1.08 |
| 1524 | (60") | 1.20 |


| Capacity multiplying factors <br> for motive gas supply (other than steam) |  |  |  |  |  |  |  |  |  |
| :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- |
| \% Back <br> pressure <br> v. <br> Motive <br> pressure <br> (bp/MP) | $10 \%$ | $20 \%$ | $30 \%$ | $40 \%$ | $50 \%$ | $60 \%$ | $70 \%$ | $80 \%$ | $90 \%$ |
| Capacity <br> multiplying <br> factors | 1.19 | 1.43 | 1.43 | 1.53 | 1.85 | 2.04 | 2.14 | 2.20 | 2.44 |

## Condensate pumps

Mechanical pumps and pumps traps

## To size the PTF4 in a closed system:

Please note that the vent assist valve that is noted in the formula below can be identified by item 23 on page 1 .
Establish the available motive pressure.
Establish the static backpressure on the pump-trap combination.
Place the established pressures into the formula below:

- Pump motive pressure - Minimum valve assist valve delta $P$ > Backpressure
- Capacity charts to be read as normal, i.e. at pump motive and backpressure.
- If, Pump motive pressure - Minimum valve assist valve delta $P$ < Backpressure, then isolate or remove the valve assist valve and multiply the capacity by 0.77 to find the reduced capacity without the valve assist valve.


## Sizing example: 1

A closed system has the following conditions:
Motive steam available $=10.3$ bar g ( 150 psig ). Static backpressure $=3.1 \mathrm{barg}(45 \mathrm{psig})$.
Open system
PTF4 capacity charts show capacity at 10.3 bar $\mathrm{g}(150 \mathrm{psi} \mathrm{g})$ motive with 3.1 bar $\mathrm{g}(45 \mathrm{psig})$ backpressure.

## Closed system

The vent assist valve on the PTF4 requires at least 5.2 bar $\mathrm{g}(75 \mathrm{psig})$ differential pressure to operate in a closed system.

## To size the PTF4 pump:

Pump motive pressure - Minimum valve assist valve delta P > Backpressure
$10.3 \operatorname{barg}(150 \mathrm{psig})-5.2$ bar g ( 75 psi g$)>3.1$ barg ( 45 psig )
As the motive pressure is 10.3 bar $\mathrm{g}(150 \mathrm{psig})$ and the valve assist valve requires a minimum 8.3 bar $\mathrm{g}(120 \mathrm{psi} \mathrm{g})$ to operate:
$5.2+3.1=8.3$ bar $\mathrm{g}(75+45=120 \mathrm{psi} \mathrm{g})$, this combination is sized correctly.

| Motive pressure |  | Backpressure |  | Condensate capacity |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| bar g | psig | bar g | psig | kg/h | lb/h |
| 13.8 | 200 | 10.3 | 150 | 10055 | 22120 |
| 13.8 | 200 | 9.7 | 140 | 10441 | 22970 |
| 13.8 | 200 | 8.3 | 120 | 11305 | 24870 |
| 13.8 | 200 | 6.9 | 100 | 12323 | 27110 |
| 13.8 | 200 | 5.5 | 80 | 13573 | 29860 |
| 13.8 | 200 | 4.1 | 60 | 15182 | 33400 |
| 13.8 | 200 | 3.4 | 50 | 16200 | 35640 |
| 13.8 | 200 | 2.8 | 40 | 17450 | 38390 |
| 13.8 | 200 | 2.1 | 30 | 19059 | 41930 |
| 13.8 | 200 | 1.4 | 20 | 21327 | 46920 |
| 13.8 | 200 | 1.0 | 15 | 22936 | 50460 |
| 12.4 | 180 | 8.3 | 120 | 10773 | 23700 |
| 12.4 | 180 | 6.9 | 100 | 11827 | 26020 |
| 12.4 | 180 | 5.5 | 80 | 13114 | 28850 |
| 12.4 | 180 | 4.1 | 60 | 14773 | 32500 |
| 12.4 | 180 | 3.4 | 50 | 15823 | 34810 |
| 12.4 | 180 | 2.8 | 40 | 17109 | 37640 |
| 12.4 | 180 | 2.1 | 30 | 18773 | 41300 |
| 12.4 | 180 | 1.4 | 20 | 21109 | 46440 |
| 12.4 | 180 | 1.0 | 15 | 22768 | 50090 |
| 11.0 | 160 | 8.3 | 120 | 10241 | 22530 |
| 11.0 | 160 | 6.9 | 100 | 11327 | 24920 |
| 11.0 | 160 | 5.5 | 80 | 12650 | 27830 |
| 11.0 | 160 | 4.1 | 60 | 14359 | 31590 |
| 11.0 | 160 | 3.4 | 50 | 15445 | 33980 |
| 11.0 | 160 | 2.8 | 40 | 16768 | 36890 |
| 11.0 | 160 | 2.1 | 30 | 18482 | 40660 |
| 11.0 | 160 | 1.4 | 20 | 20891 | 45960 |
| 11.0 | 160 | 1.0 | 15 | 22600 | 49720 |
| 9.7 | 140 | 6.9 | 100 | 10641 | 23410 |
| 9.7 | 140 | 5.5 | 80 | 11918 | 26220 |
| 9.7 | 140 | 4.1 | 60 | 13568 | 29850 |
| 9.7 | 140 | 3.4 | 50 | 14614 | 32150 |
| 9.7 | 140 | 2.8 | 40 | 15891 | 34960 |
| 9.7 | 140 | 2.1 | 30 | 17541 | 38590 |
| 9.7 | 140 | 1.4 | 20 | 19868 | 43710 |
| 9.7 | 140 | 1.0 | 15 | 21518 | 47340 |
| 8.3 | 120 | 5.5 | 80 | 11186 | 24610 |
| 8.3 | 120 | 4.1 | 60 | 12777 | 28110 |


| Motive pressure |  | Backpressure |  | Condensate capacity |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| bar g | psig | bar g | psig | kg/h | lb/h |
| 8.3 | 120 | 3.4 | 50 | 13782 | 30320 |
| 8.3 | 120 | 2.8 | 40 | 15014 | 33030 |
| 8.3 | 120 | 2.1 | 30 | 16605 | 36530 |
| 8.3 | 120 | 1.4 | 20 | 18845 | 41460 |
| 8.3 | 120 | 1.0 | 15 | 20432 | 44950 |
| 6.9 | 100 | 4.1 | 60 | 11241 | 24730 |
| 6.9 | 100 | 3.4 | 50 | 12318 | 27100 |
| 6.9 | 100 | 2.8 | 40 | 13641 | 30010 |
| 6.9 | 100 | 2.1 | 30 | 15341 | 33750 |
| 6.9 | 100 | 1.4 | 20 | 17741 | 39030 |
| 6.9 | 100 | 1.0 | 15 | 19445 | 42780 |
| 5.5 | 80 | 4.1 | 60 | 9705 | 21350 |
| 5.5 | 80 | 3.4 | 50 | 10855 | 23880 |
| 5.5 | 80 | 2.8 | 40 | 12264 | 26980 |
| 5.5 | 80 | 2.1 | 30 | 14077 | 30970 |
| 5.5 | 80 | 1.4 | 20 | 16641 | 36610 |
| 5.5 | 80 | 1.0 | 15 | 18455 | 40600 |
| 4.8 | 70 | 3.4 | 50 | 9932 | 21850 |
| 4.8 | 70 | 2.8 | 40 | 11286 | 24830 |
| 4.8 | 70 | 2.1 | 30 | 13036 | 28680 |
| 4.8 | 70 | 1.7 | 25 | 14145 | 31120 |
| 4.8 | 70 | 1.4 | 20 | 15505 | 34110 |
| 4.8 | 70 | 1.0 | 15 | 17255 | 37960 |
| 4.1 | 60 | 2.8 | 40 | 10427 | 22940 |
| 4.1 | 60 | 2.1 | 30 | 12200 | 26840 |
| 4.1 | 60 | 1.7 | 25 | 13323 | 29310 |
| 4.1 | 60 | 1.4 | 20 | 14695 | 32330 |
| 4.1 | 60 | 1.0 | 15 | 16468 | 36230 |
| 3.4 | 50 | 2.1 | 30 | 11505 | 25310 |
| 3.4 | 50 | 1.7 | 25 | 12714 | 27970 |
| 3.4 | 50 | 1.4 | 20 | 14050 | 30910 |
| 3.4 | 50 | 1.0 | 15 | 15527 | 34160 |
| 2.8 | 40 | 2.1 | 30 | 8855 | 19480 |
| 2.8 | 40 | 1.7 | 25 | 10105 | 22230 |
| 2.8 | 40 | 1.4 | 20 | 11636 | 25600 |
| 2.8 | 40 | 1.0 | 15 | 13609 | 29940 |
| 2.1 | 30 | 1.4 | 20 | 9291 | 20440 |
| 2.1 | 30 | 1.0 | 15 | 11659 | 25650 |

Assumes a Fill Head - 1.42m (36"), Fill Height - 2.86 m (70")

## Capacity charts



## Condensate pumps



PTF4 Pivotrol ${ }^{\circledR}$ steam consumption chart
Backpressure (psig)

PTF4 Pivotrol ${ }^{\circledR}$ air consumption chart

## How to order

## Sample specification

The pump shall be Spirax Sarco Pivotrol ${ }^{\circledR}$ Pump (patented) Dual Mechanism PTF4, operated by steam, compressed air or other pressurised gas to 13.8 bar $g(200 \mathrm{psi} \mathrm{g})$, which does not require any electrical energy, and is capable of pumping liquids down to 0.88 specific gravity. The pump shall have stainless steel, split disc check valves on the inlet and outlet connections. The pump shall contain Spirax Sarco PowerPivot ${ }^{\circledR}$ (patented) technology to ensure longevity and reliability of the pump. The Pivotrol ${ }^{\circledR}$ Pump shall include an Inconel spring with a lifetime warranty and be supplied with an integral cycle counter to monitor a 3 million cycle $\times 3$ year warranty. When required the pump shall be supplied with a reflex gauge glass.

## Safety information, installation and maintenance

For full details see the Installation and Maintenance Instructions (IM-P135-14) supplied with the product.


[^0]:    Maximum number of cycles per minute $=6$

